

## GESTRA Steam Systems

## Product Range A4

### Control Valve With Radial Stage Nozzle ZK and Tandem Shut-Off **ZK 213** DN 80 – 250

### ZK 213

#### Description

Control valve for operation at very high differential pressures.

Application, for example, in industrial plants and power stations as

- Leak-off valve for condensate pumps etc.
- Injection-cooling valve
- Start-up pot drain valve
- Feedwater control valve

The pressure drop is decreased in the radial stage nozzle ZK in several stages, so that the flow velocity is reduced leading to a considerable reduction in wear and noise (sound level  $\leq 85$  dB(A)).

The dual (tandem) shut-off combines the function of a conventional shut-off valve and a valve provided with regulating cone. At the beginning of the opening process first the main valve plug is lifted off the main seat, while the secondary valve plug remains closed until the main plug has reached a certain lift. At the moment of closing and at the beginning of opening the flow velocity at the valve seat is therefore zero so that wire drawing is excluded.

Angle-type or Z-type valve body.

The valve permits the use of several actuator types:

1. ZK 213-.../13  
Electric linear actuator
2. ZK 213-.../14  
Design with insert bush for fitting an electric rotary actuator or a handwheel
3. ZK 213-.../20  
Pneumatic diaphragm actuator
4. ZK 213-.../40  
Hydraulic linear actuator

**Example:** ZK 213-E2/14

- E = angle version  
(Z = Z-type version)
- 2 = size  
see table "k<sub>vs</sub>-value"
- 14 = type of actuator  
(13, 14, 20, 40)

Internals completely exchangeable (incl. seat).

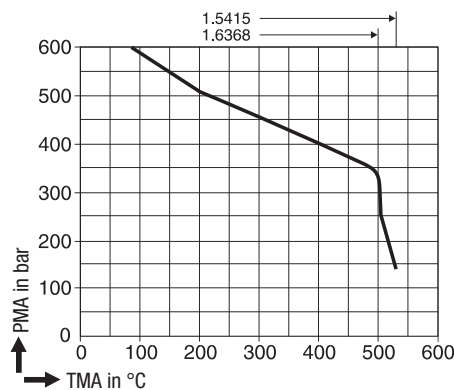
Leak rate acc. to DIN 3230 BN 1.

#### Pressure/Temperature Rating with materials

1.5415		1.6368	
bar	°C	bar	°C
psig	°F	psig	°F
510	200	510	200
7400	392	7400	392
450	300	450	300
6530	572	6530	572
400	400	400	400
5800	752	5800	752
280	500	280	500
4060	932	4060	932
136	530		
1970	985		

#### Differential pressure

- ΔPMX 300 bar (4350 psi) – 4 stages
- 560 bar (8120 psi) – 6 stages

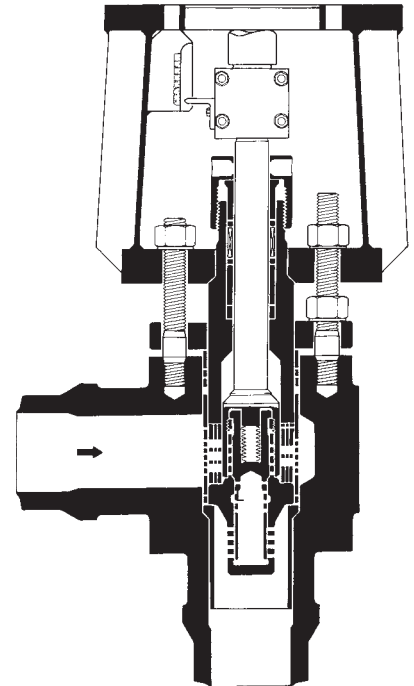


#### Materials

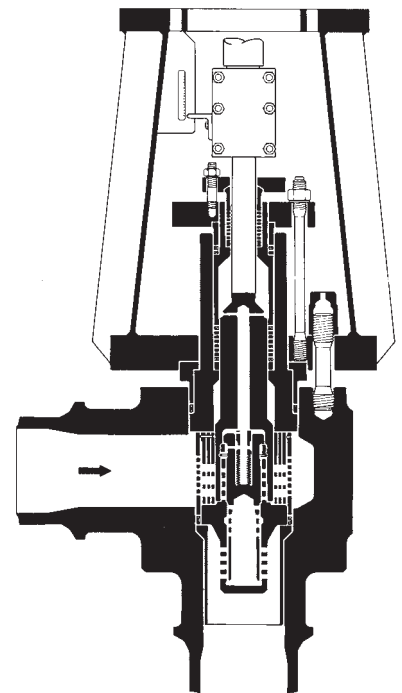
Body	Forged alloy steel 15 Mo3 (1.5415) or WB 36 (1.6368)
Internals	s.s. X35CrMo 17 (1.4122) s.s. X90CrMoV 18 (1.4112) s.s. X20CrMoV 12 1 (1.4922)
Gland packing	Pure graphite

#### Connections

Butt-weld ends. Dimensions on request.

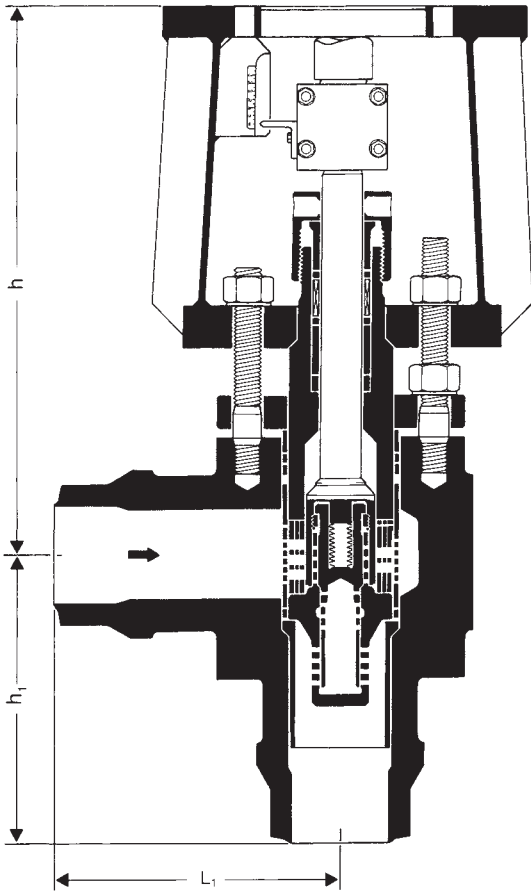


ZK 213  
Sizes 1 and 2

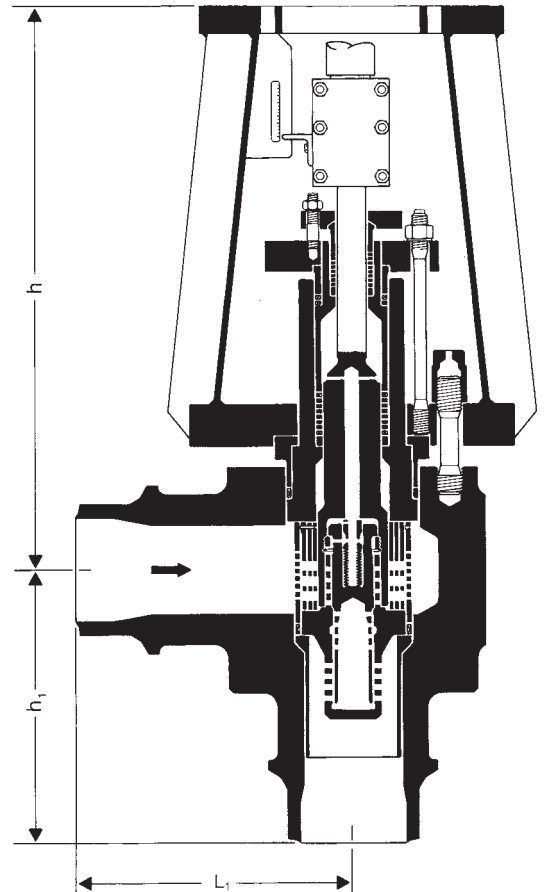


ZK 213  
Sizes 3 and 4,  
partially balanced

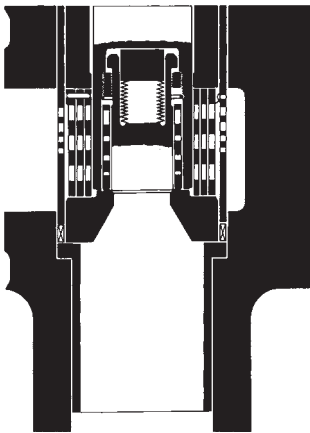
## Dimensions



ZK 213-E.../...  
Sizes 1 and 2  
6 stages



ZK 213-E.../...  
Sizes 3 and 4  
6 stages,  
partially balanced



ZK 213  
4 stages

Size	1	2	3	4
DN mm (in)	180 (3) 100 (4) 125 (5)	100 (4) 125 (5) 150 (6)	125 (5) 150 (6) 200 (8)	150 200 250
h	635	735	890	910
h <sub>1</sub>	260	350	400	400
L <sub>1</sub>	260	350	400	400
Weight [kg]	210	370	540	600

### Calculation of required $k_v$ value\*)

- For water flowrates within temperature ranges where flashing because of pressure drop is not to be expected (e.g. leak-off and injection-cooling valves) the calculated  $k_v$  value has to be multiplied by a correction factor taken from the chart below due to the successive expansion. The chart includes a safety factor of 1.2.
- If, due to the pressure drop, flashing is to be expected, the formulae below should not be used to calculate the  $k_v$  value. In this case see overleaf for hot water capacity charts. If  $p_2/p_1 > 0.5$  multiply the chart reading by the correction factor K taken from the back pressure chart below. The safety factor of 1.2 must always be taken into consideration.
- For steam the calculated  $k_v$  value has to be multiplied by a safety factor of 1.2.

Pressure drop	$k_v$	for liquids	for gas, temperature-corrected	for vapours	for saturated and wet steam
$\Delta p < \frac{p_1}{2}$ $\left( p_2 > \frac{p_1}{2} \right)$	$k_v$	$= \frac{\dot{V}}{31.6} \sqrt{\frac{\rho_1}{\Delta p}}$	$= \frac{\dot{V}_N}{514} \sqrt{\frac{\rho_N \cdot T_1}{\Delta p \cdot p_2}}$	$= \frac{\dot{m}}{31.6} \sqrt{\frac{v}{\Delta p}}$	$= \frac{\dot{m}}{31.6} \sqrt{\frac{v \cdot x}{\Delta p}}$
$\Delta p > \frac{p_1}{2}$ $\left( p_2 < \frac{p_1}{2} \right)$	$k_v$	$= \frac{\dot{m}}{31.6 \sqrt{\rho_1 \cdot \Delta p}}$	$= \frac{2 \dot{V}_N}{514 \cdot p_1} \sqrt{\rho_N \cdot T_1}$	$= \frac{\dot{m}}{31.6} \sqrt{\frac{2v}{p_1}}$	$= \frac{\dot{m}}{31.6} \sqrt{\frac{v \cdot x \cdot 2}{p_1}}$

\*) Conversion Factors:  $C_v$  (U.S.) = 1.17 ·  $k_v$      $C_v$  (U.K.) = 0.98 ·  $k_v$

#### Nomenclature:

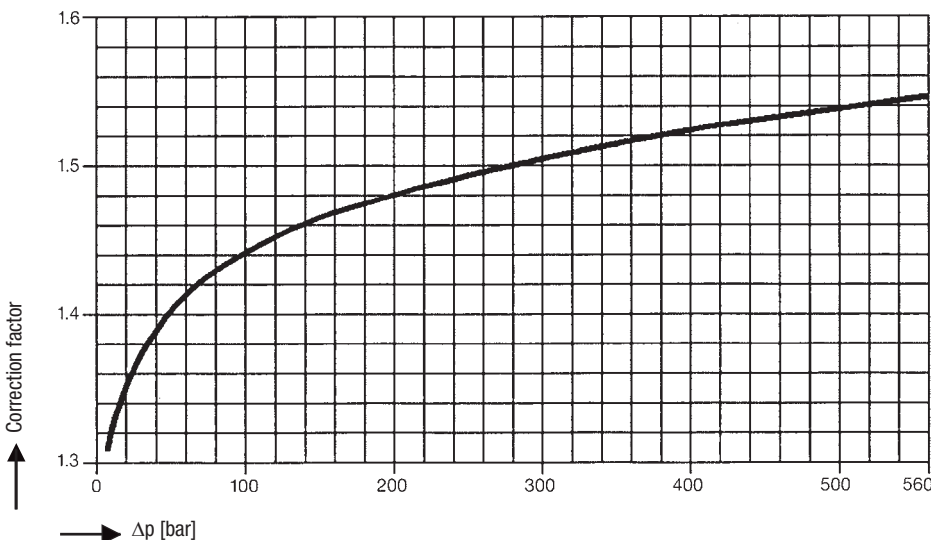
$k_v$	Value flow coefficient for fully open valve within control range	[m <sup>3</sup> /h]	$\Delta p$	Pressure drop $p_1 - p_2$	[bar]
$\dot{V}$	Flowrate	[m <sup>3</sup> /h]	$\rho_1$	Density of fluid with operating condition at $T_1$ and $p_2$	[kg/m <sup>3</sup> ]
$\dot{m}$	Flowrate	[kg/h]	$\rho_N$	Density of gases at standard state (0°C, 1013 mbar)	[kg/m <sup>3</sup> ]
$\dot{V}_N$	Volume flowrate for gases at standard state (0°C, 1013 mbar)	[m <sup>3</sup> /h]	$v$	Specific steam volume at $T_1$ and $p_2$ or – if $\Delta p > \frac{p_1}{2}$ – at $\frac{p_1}{2}$	[m <sup>3</sup> /kg]
$p_1$	Upstream pressure	[bar a]	$T_1$	Absolute inlet temperature of fluid	[K]
$p_2$	Downstream pressure	[bar a]	$x$	Content of dry saturated steam in wet steam	(0 < $x$ ≤ 1)

### $K_v$ Values at Control Stroke $H_{100}$

See page 4: The characteristic lines in the upper part of the chart indicate simultaneously the  $k_v$  values.

	DN	$k_v$ values [m <sup>3</sup> /h]		Control stroke $H_{100}$ [mm]
		4 stages $\Delta p_{\max}$ 300 bar (4350 psi)	6 stages $\Delta p_{\max}$ 560 bar (8120 psi)	
ZK 213-...1/...	80 – 125 mm (3 – 5")	13	10	50
ZK 213-...2/...	100 – 150 mm (4 – 6")	26	20	60
ZK 213-...3/...	125 – 200 mm (5 – 8")	39	30	70
ZK 213-...4/...	150 – 250 mm (6 – 10")	60	46	70

### Correction factor for water flowrates (without flashing)



**Control Valve**  
**With Radial Stage Nozzle ZK and**  
**Tandem Shut-Off**  
**ZK 213**  
**DN 80 – 250**

**Order and Enquiry Specifications**

Control valve with radial stage nozzle ZK and tandem shut-off ZK 213.

Design data:  $p = \dots$  bar  $t = \dots$  °C

Operational data: Load Conditions (1 – 3)

	1	2	3
$p_1$ [bar]			
$t_1$ [°C]			
$p_2$ [bar]			
$\Delta p$ [bar]			
$\dot{m}$ [t/h]			

Please enter data in this table.

Fluid: .....

Actuators: Electric (make)  
 On-off or modulating control  
 Voltage/Hz.../...  
 Control voltage/Hz.../...  
 for electro-hydraulic  
 linear actuators indicate  
 on-off or modulating control  
 $\Delta p$  max in bar for sizing of  
 actuator

The following test certificates can be issued on request, at extra cost:

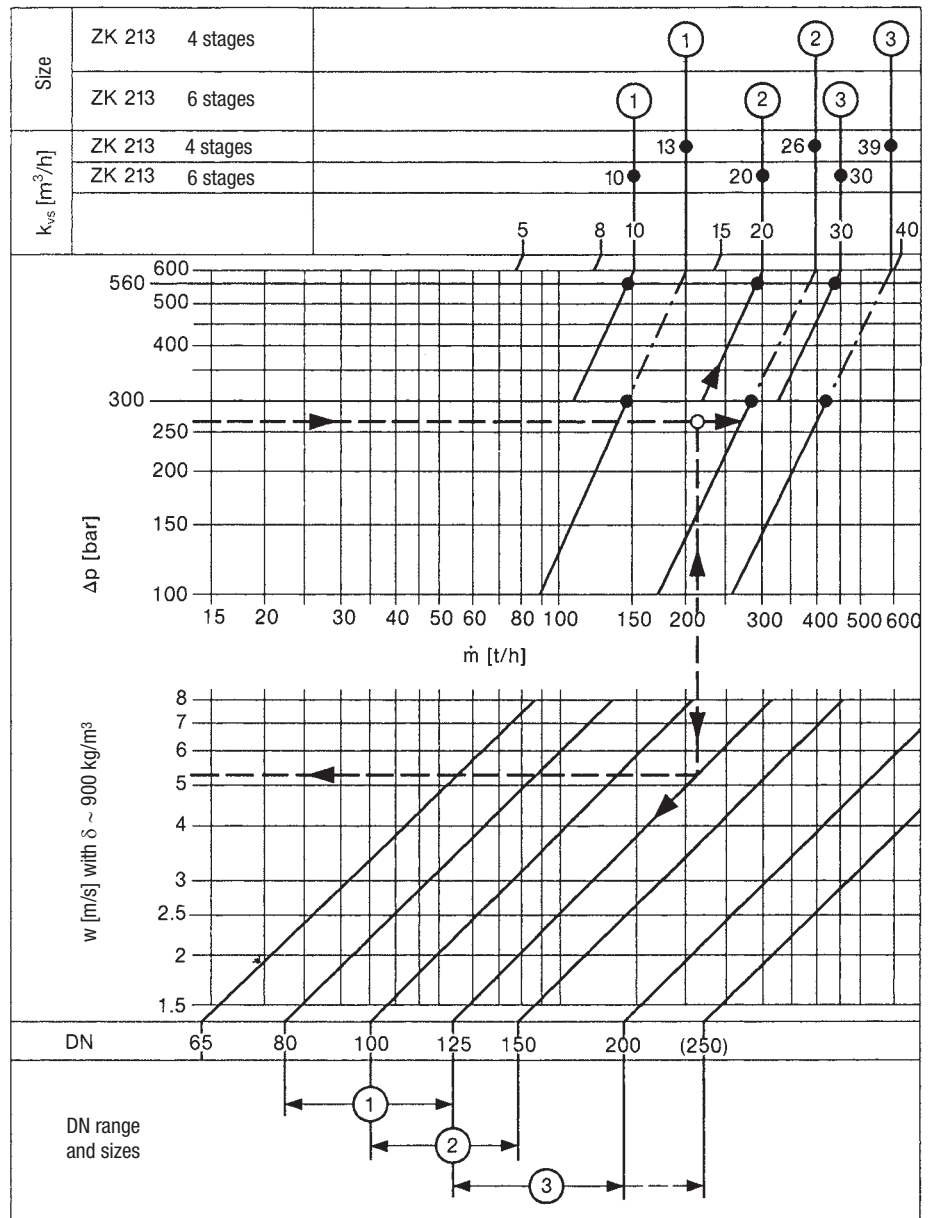
In accordance with EN 10204/-2.1, -2.2, -3.1A, -3.1B and -3.1C.

All inspection requirements have to be stated with the order. After supply of the equipment certificates can no longer be established. Charges and extent of the above mentioned certificates as well as the different tests confirmed therein are listed in our leaflet "Test and Inspection Charges for Standard Equipment". For other tests and inspections than those listed above, please consult us.

Supply in accordance with our general terms of business.

**Leak-off valves ZK 213**

Chart for determination of size, nominal size and flow velocity  $v$  in the pipe



**Example: Sizing of a leak-off valve.**

Operating conditions:  
 Upstream pressure  $p_1 = 285$  bar      Feedwater temperature  $t = 210$  °C  
 Back pressure  $p_2 = 15$  bar      Flowrate  $\dot{m} = 210$  t/h

Differential pressure across the leak-off valve  $\Delta p = 270$  bar (upstream pressure minus back pressure)

In accordance with the above chart, the required  $k_v$  value for a flowrate of 210 t/h is 20 m<sup>3</sup>/h.

Since the differential pressure  $\Delta p$  is lower than 300 bar, the ZK 213 with 4 stages, size 2, with a  $k_v$  value of 26 m<sup>3</sup>/h is selected.

For each valve size 3 different nominal sizes are available; for size 2 these are DN 100, 125 and 150 (4, 5 and 6").

For leak-off lines we recommend flow velocities between 4 and 8 m/s.

From the lower part of the chart indicating the flow velocities we can read a velocity of 5.4 m/s for DN 125, i.e. DN 125 mm should be selected.

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